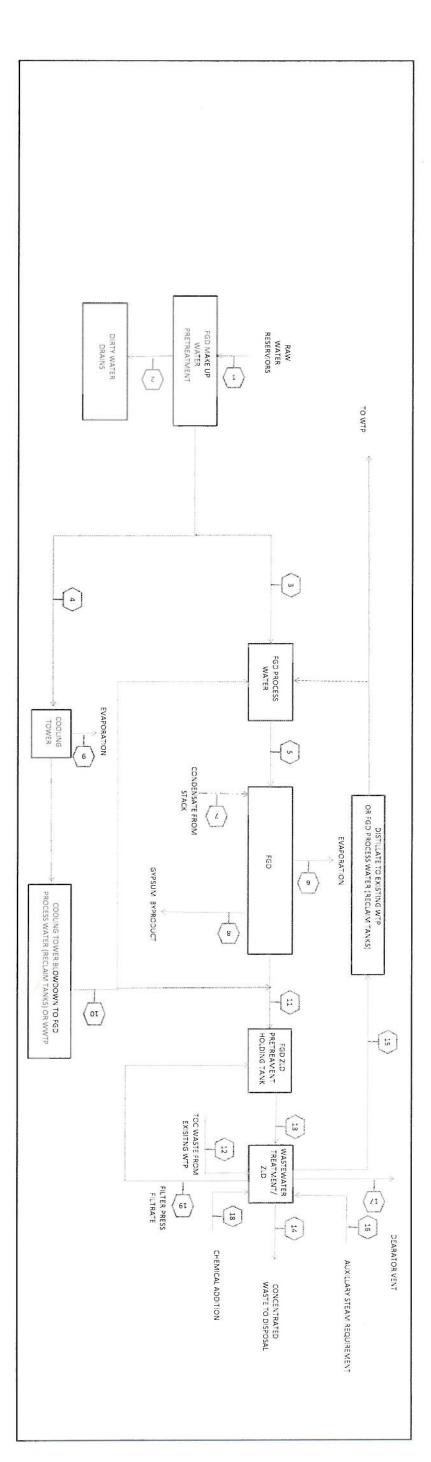
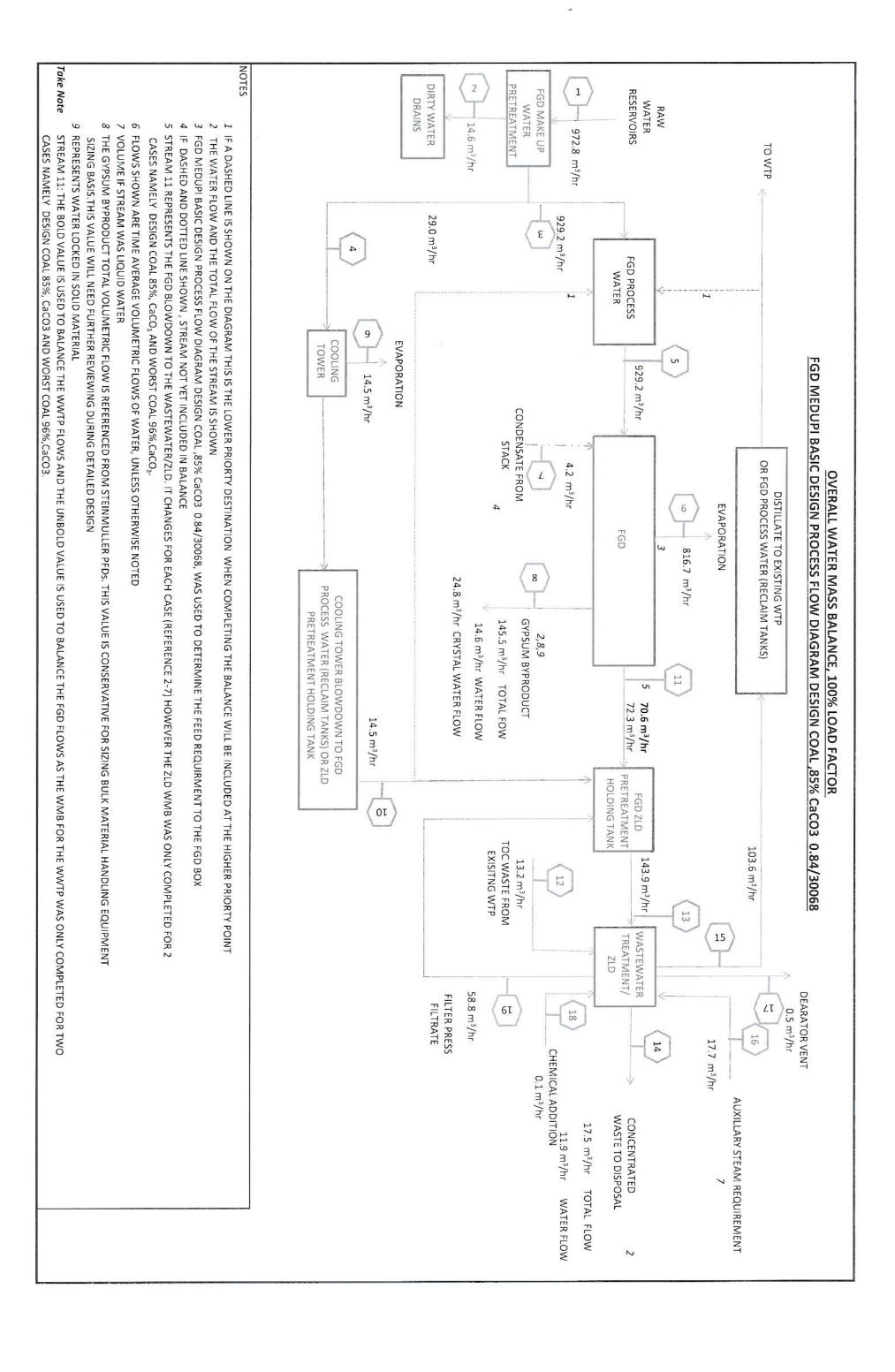
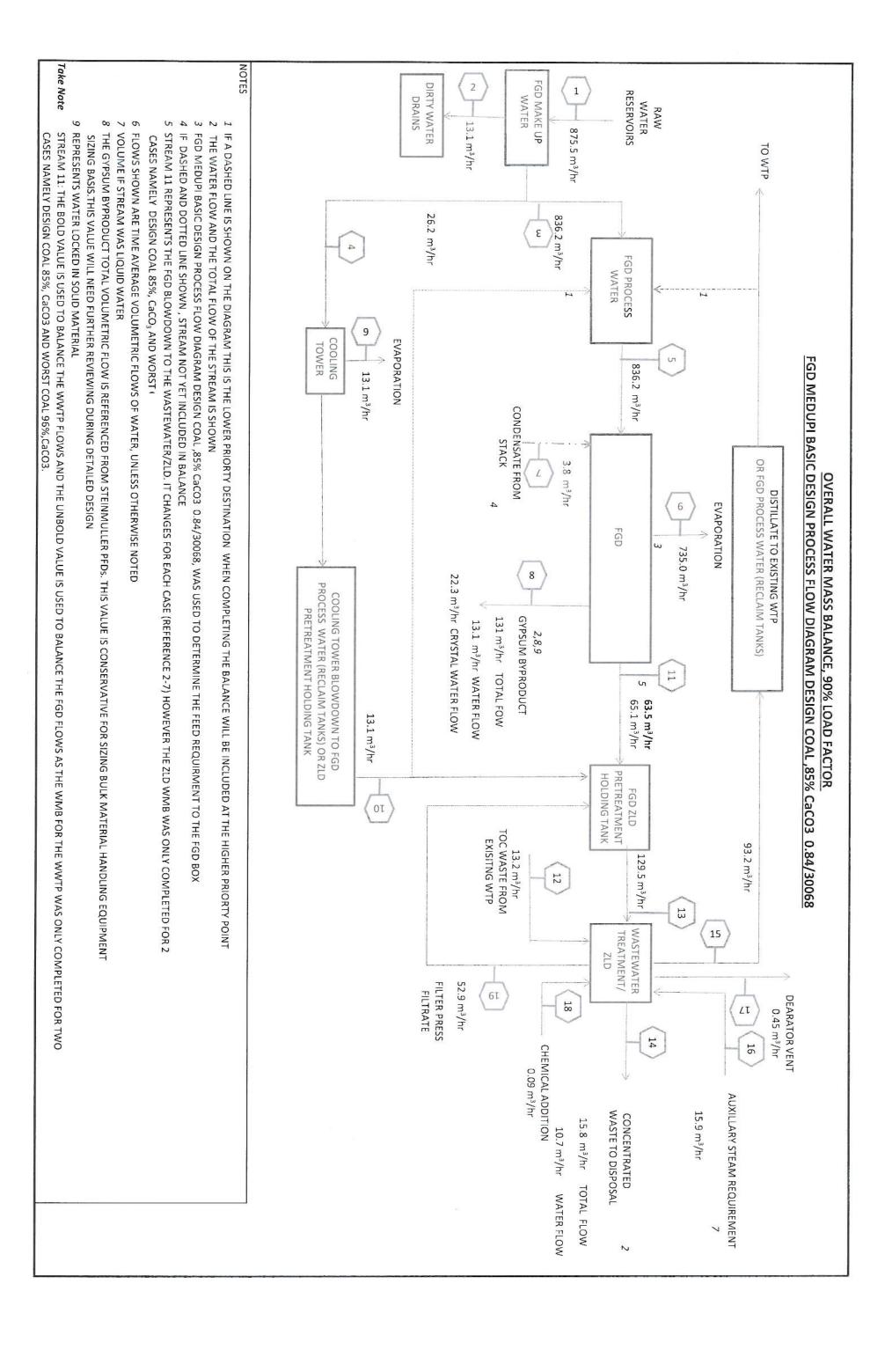
		MEDUPI FGD V	MEDUPI FGD WATER MASS BALANCE	ALANCE		
Company Name:	Eskom			Page	1 of	14
Project Name:	Medupi FGD Project	ject		Project No: 178771	178771	
Document Title:	Overall Water Mass Balance	ass Balance				
Document Is: (check all that apply)	ck all that apply)		Preliminary	Final		
Objective	The objective of	the following diagra	The objective of the following diagram is to estimate the overall water mass balance.	overall water ma	ss balance.	
	Unveri	fied Assumptions	Unverified Assumptions Requiring Subsequent Verification	uent Verification		
No.	As	Assumption		Verified By	By	Date
1						
ω ^						
4						
	See Page		of this document for additional assumptions	or additional assur	mptions	
Conclusion						
Worst Coal+ ATT,	Worst Coal+ ATT, 96% CaCO <sub>3</sub> will be taken as the worst case scenario for the FGD project see page 13	aken as the worst c	ase scenario for the	FGD project see	page 13	
Rev	Prepared By	Date	Verified By	Date	Approved By	Date
0	Abigail Melanie	2014/06/09	Ruchman	2014/06/09	Mhrstar.	20

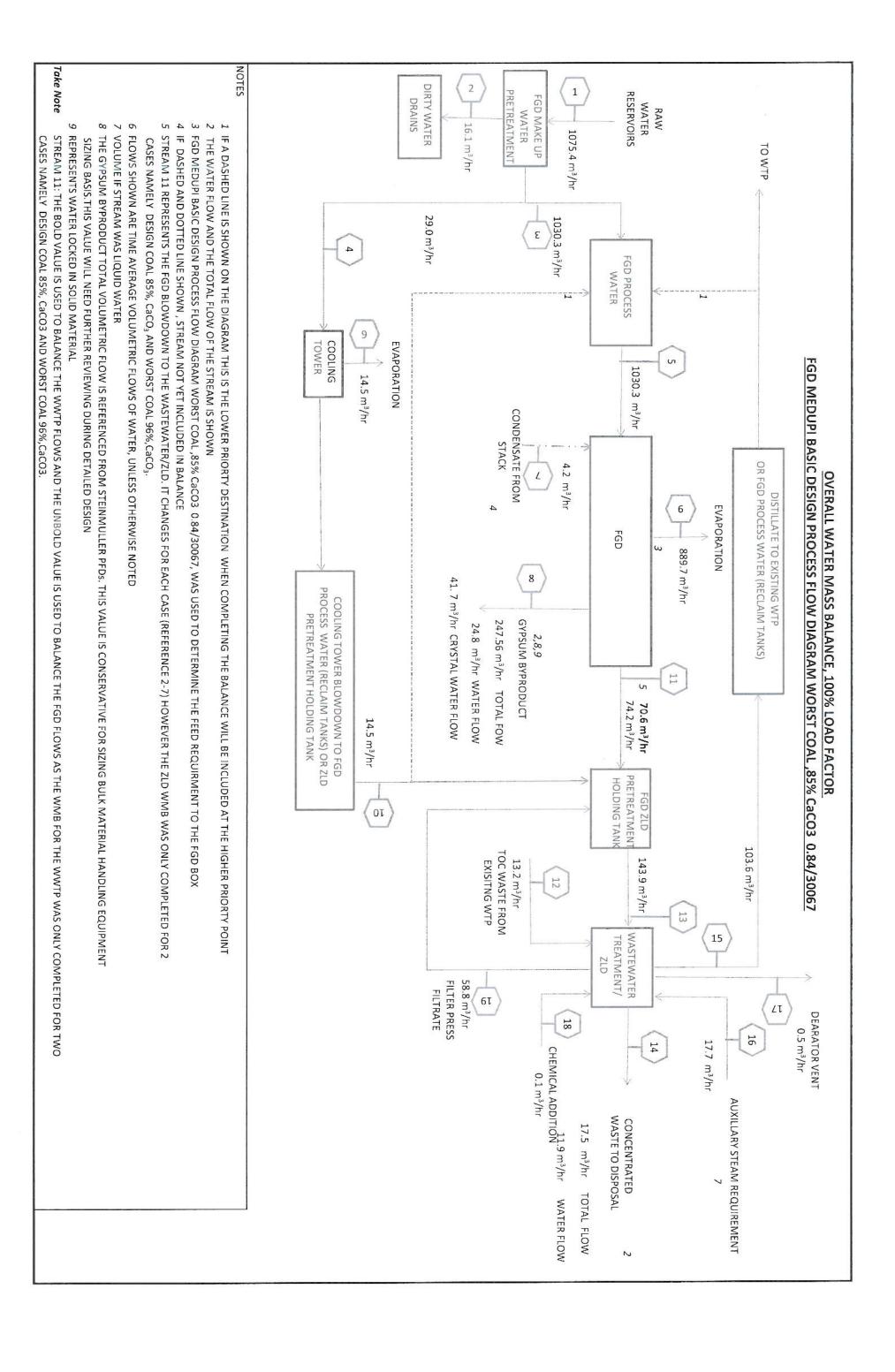
N
0
丁二
4

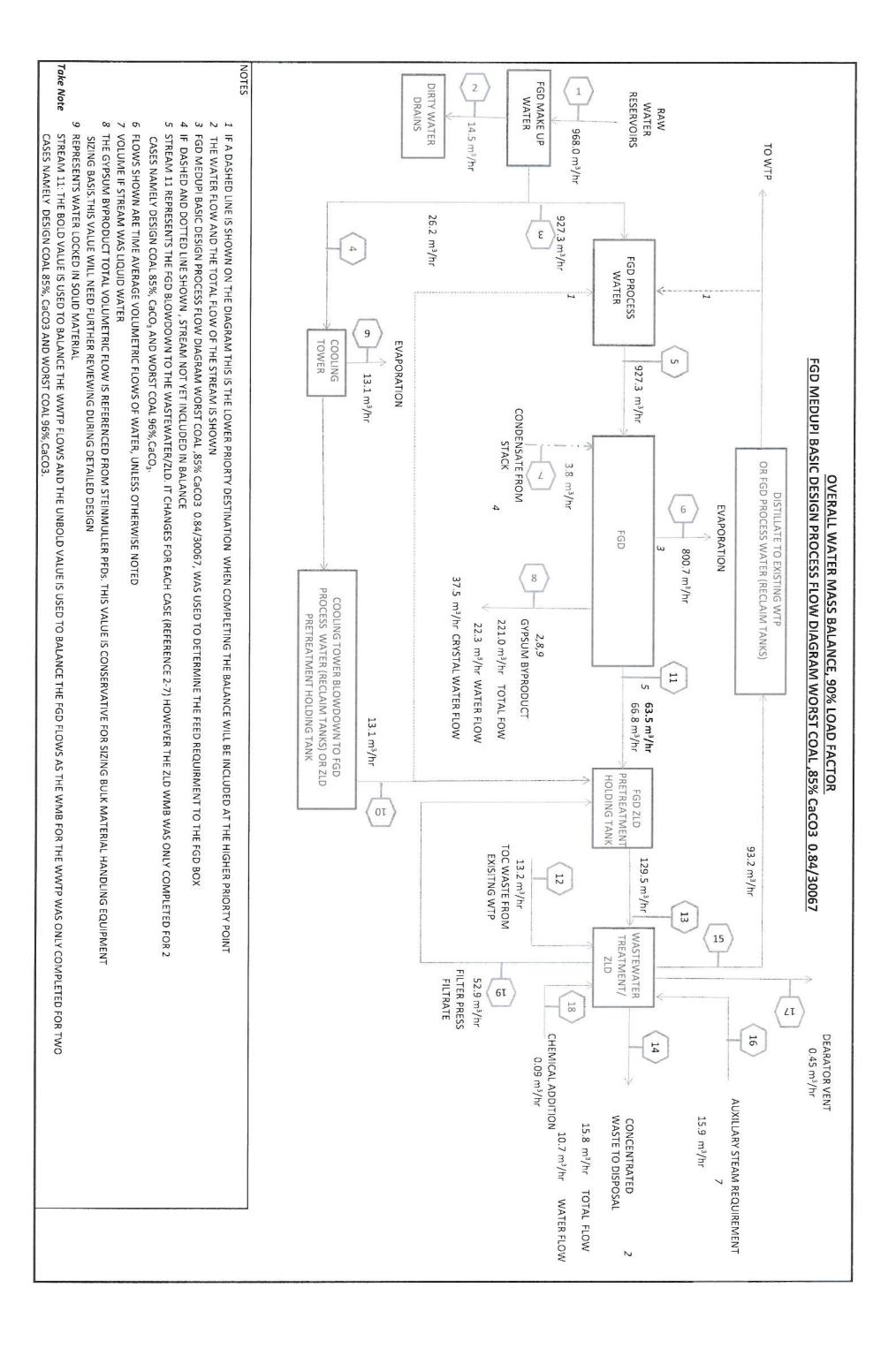
13 Total waste water into WVFP 14 Concentrated waste for disposal 15 Distillate to existing WTP or FGD make up water (reclaim tanks) 16 Auxiliary steam requirement 17 Dearator vent 18 Chemical Addition	12 I I Cou waste irrom existing W IP 13 Total waste water into WVWTP 14 Concentrated waste for disposal 15 Distillate to existing WTP or FGD make up water (reclaim tanks) 16 Auxiliary steam requirement 17 Dearator vent	12 I DC waste from existing W P 13 Total waste water into W/WTP 14 Concentrated waste for disposal 15 Distillate to existing WTP or FGD make up water (reclaim tanks) 16 Auxiliary steam requirement	12 TOC waste from existing W P  13 Total waste waste into WWTP  14 Concentrated waste for disposal  15 Distillate to existing WTP or FGD make up water (reclaim tanks)	12 IOC waste from existing WIP 13 Total waste water into WWTP 14 Concentrated waste for disposal	13 Total waste mater into WWTP	12 OC waste from existing WIP		11 FGD waste water to ZLD holding tank	10 Cooling Tower Blowdown To FGD Make up water (reclaim tanks) or WWTP	9 Cooling Tower Evaporation	8 Gypsum Byproduct	7 Condensate from the stack	6 FGD Evaporation	5 FGD make up water	4 Filtered water from pre treatment to the Cooling Tower	3 Filtered water from pre treatment to the FGD plant	2 Backwash water from pre treatment to Dirty Drains	1 Total raw water make up	Stream Nr Stream Name	13 email: "RE: 140303 56.6405 Medupi FGD - Plant FGD Water Mass Balance", Keketsi Ramahali , 2014/04/07	12 Medupi Power Station, Drain Flow Rate Design for North and South Chimney, Exponent Technical Memorandum Sept 2001: Condensate Analysis, Alden Final Report GFS- 411002-1: Condensation Calculation, Karrena-Concor Joint Venture, 10 September 2001:	11 email: "131105 56.6405 Medupi FGD - TOC analysis", Craig, Robert (Bob) M. Jr., 05/11/2013	<ol> <li>Medupi FGD, 56.6607.1202, FGD Makeup Water Pretreatment Backwashable Strainer, 15/07/2013</li> </ol>	9 Medupi FGD, 56.3202.1201, Cooling Tower Cycles of Concentration and Acid Feed Estimate, 25 October 2013	8 email: "RE: Basic Design Evaporation Rates", Candice Stephens., 03/02/2014	7 FGD Medupi Basic Design Process Flow Diagram, Worst Coal + Attemperature air,96% CaCO3 0.84/30063	6 FGD Medupi Basic Design Process Flow Diagram, Worst Coal,96% CaCO3 0.84/30054	5 FGD Medupi Basic Design Process Flow Diagram, Design Coal ,96% CaCO3 0.84/30065	4 FGD Medupi Basic Design Process Flow Diagram, Worst Coal + Attemperature Air,85% CaCO3 0.84/30066	3 FGD Medupi Basic Design Process Flow Diagram, Worst Coal,85% CaCO3 0.84/30067	2 FGD Medupi Basic Design Process Flow Diagram, Design Coal ,85% CaCO3 0.84/30068	1 Medupi FGD,56.6405.1201,FGD ZLD Water Mass Balance, 20 November 2013	References
.     .	, a   s.			1	ы	1	11	2-7	9	9	2-7 & 13	12	8	2-7	9	10	10	10	Reference	2014/04/07	ical Memorandum Sep		2013	October 2013		0.84/30063			0.84/30066				
Dependant if 85% or 96% Coal	Dependant if 85% or 96% Coal	The second of th	Dependant if 85% or 96% Coal	Dependant if 85% or 96% Coal	Dependant if 85% or 96% Coal	Dependant if 85% or 96% Coal		This is depended on the specific case			This is depended on the specific case			This is depended on the specific case		Modification applied for each specific case (ref 2-6)	Modification applied for each specific case (ref 2-6)	Modification applied for each specific case (ref 2- 6)	Comment		t 2001: Condensate Analysis, Alden Final Report GFS- 41												
																					411002-1: Condensation Calculation, Karrena-Concor Joint Venture, 10 September 2001												

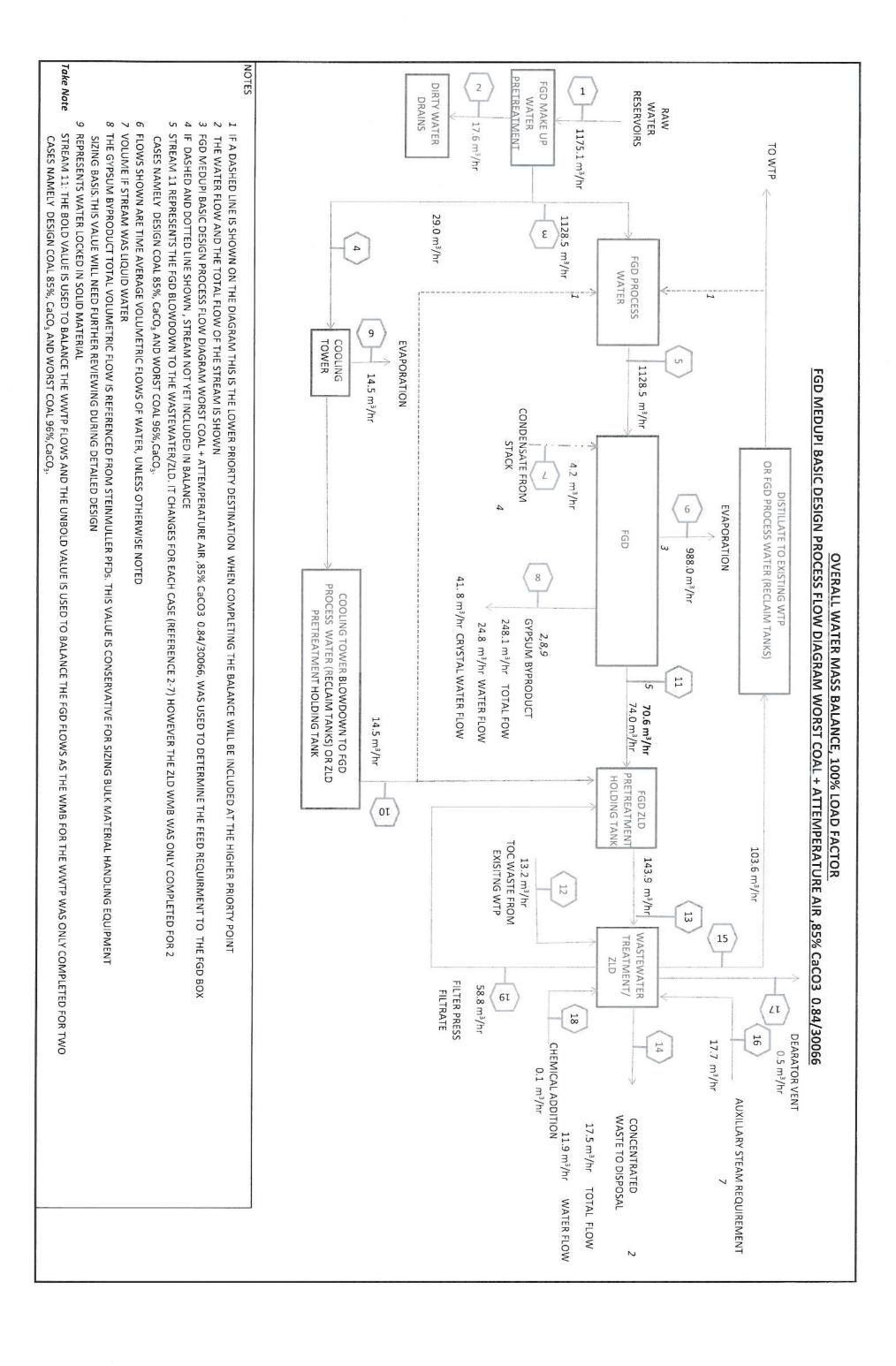


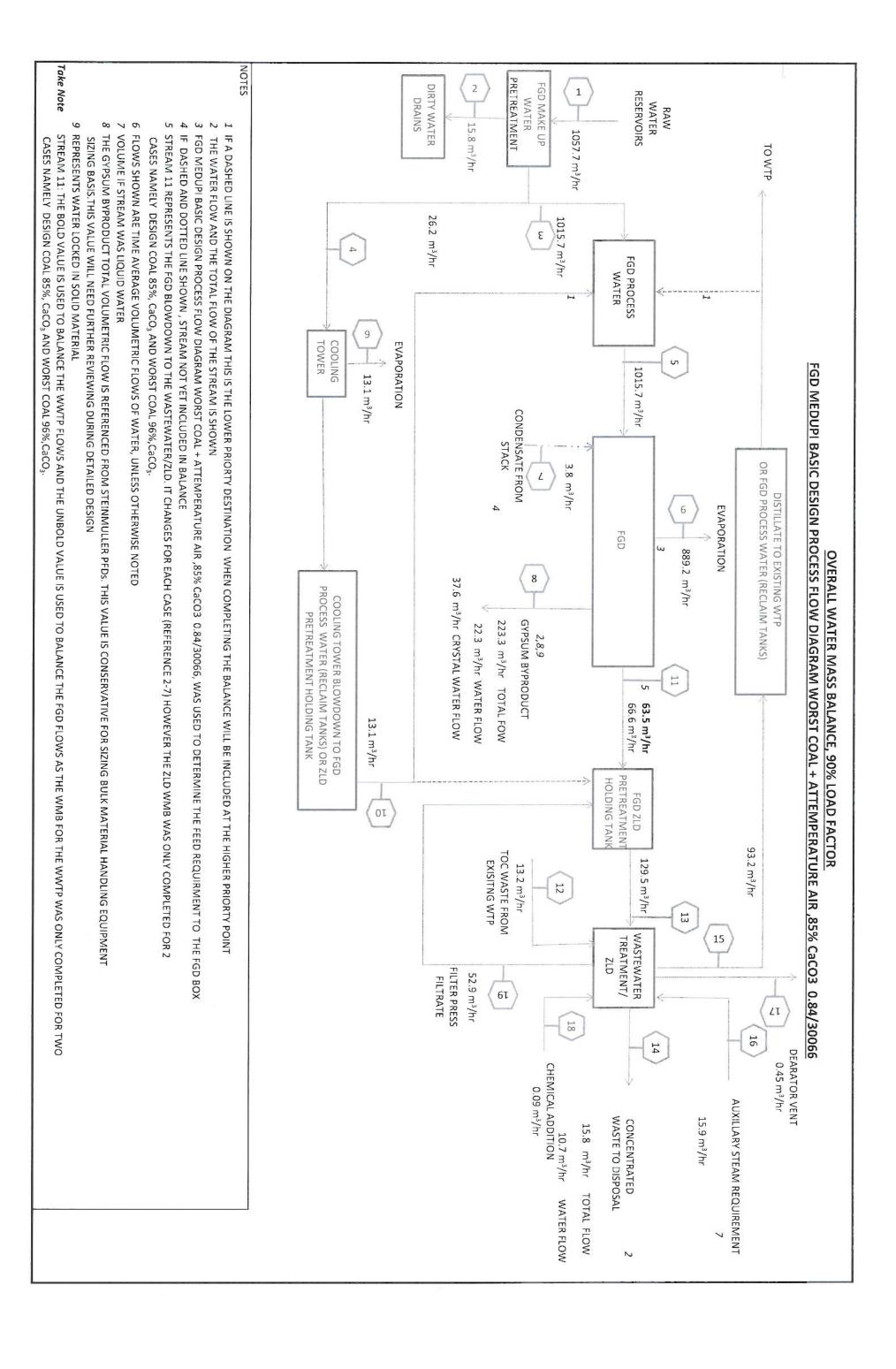


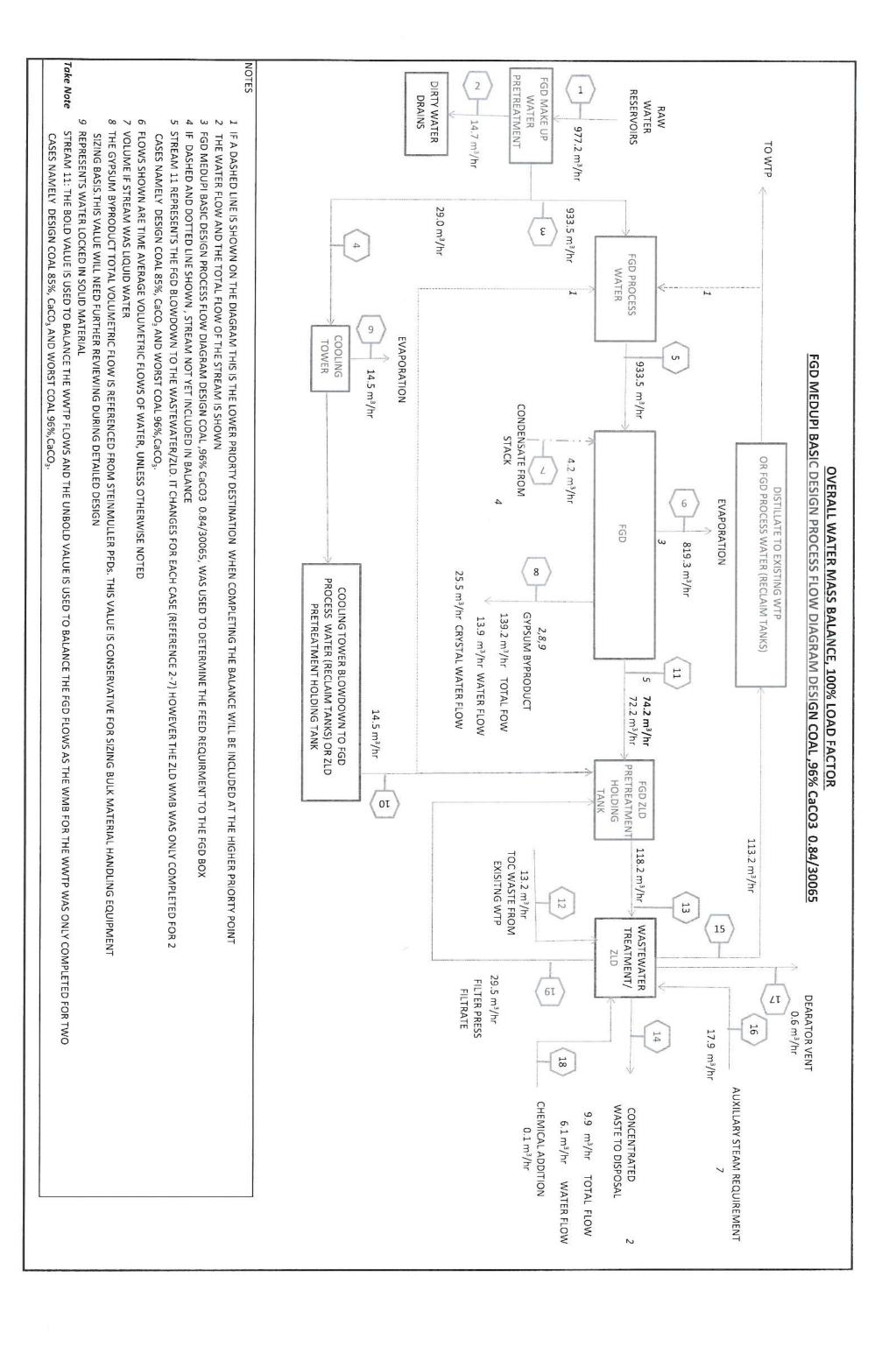


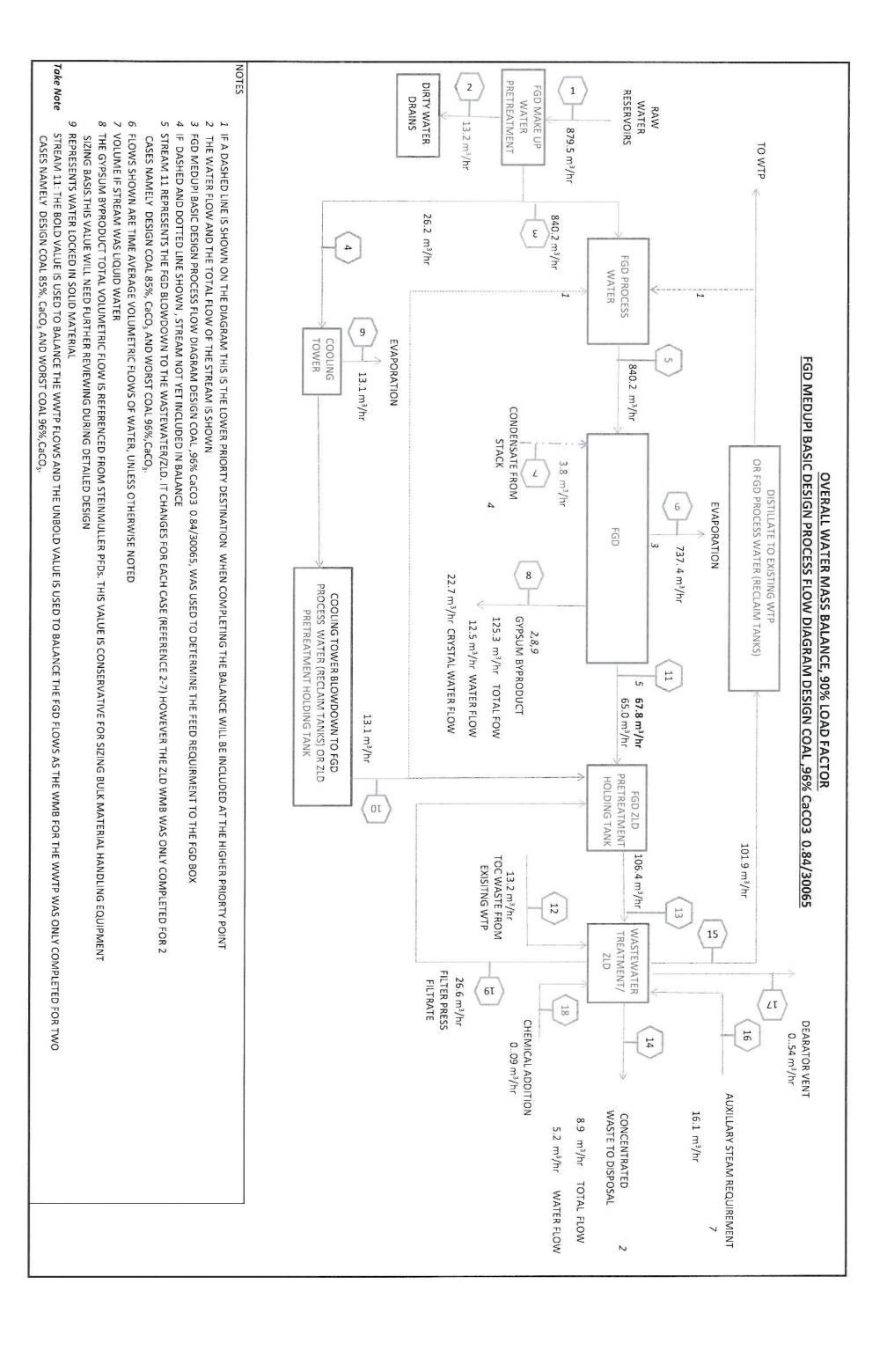


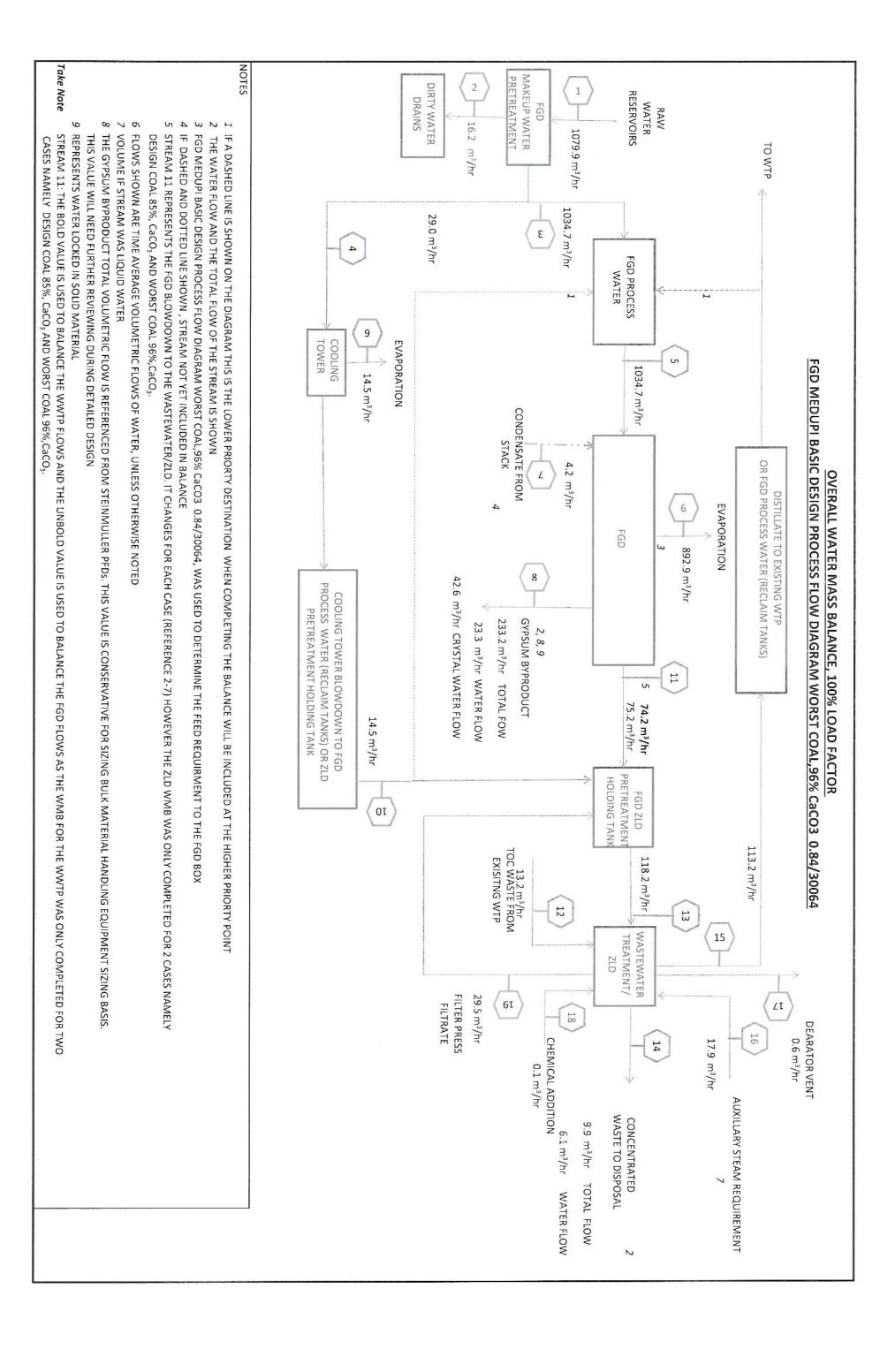


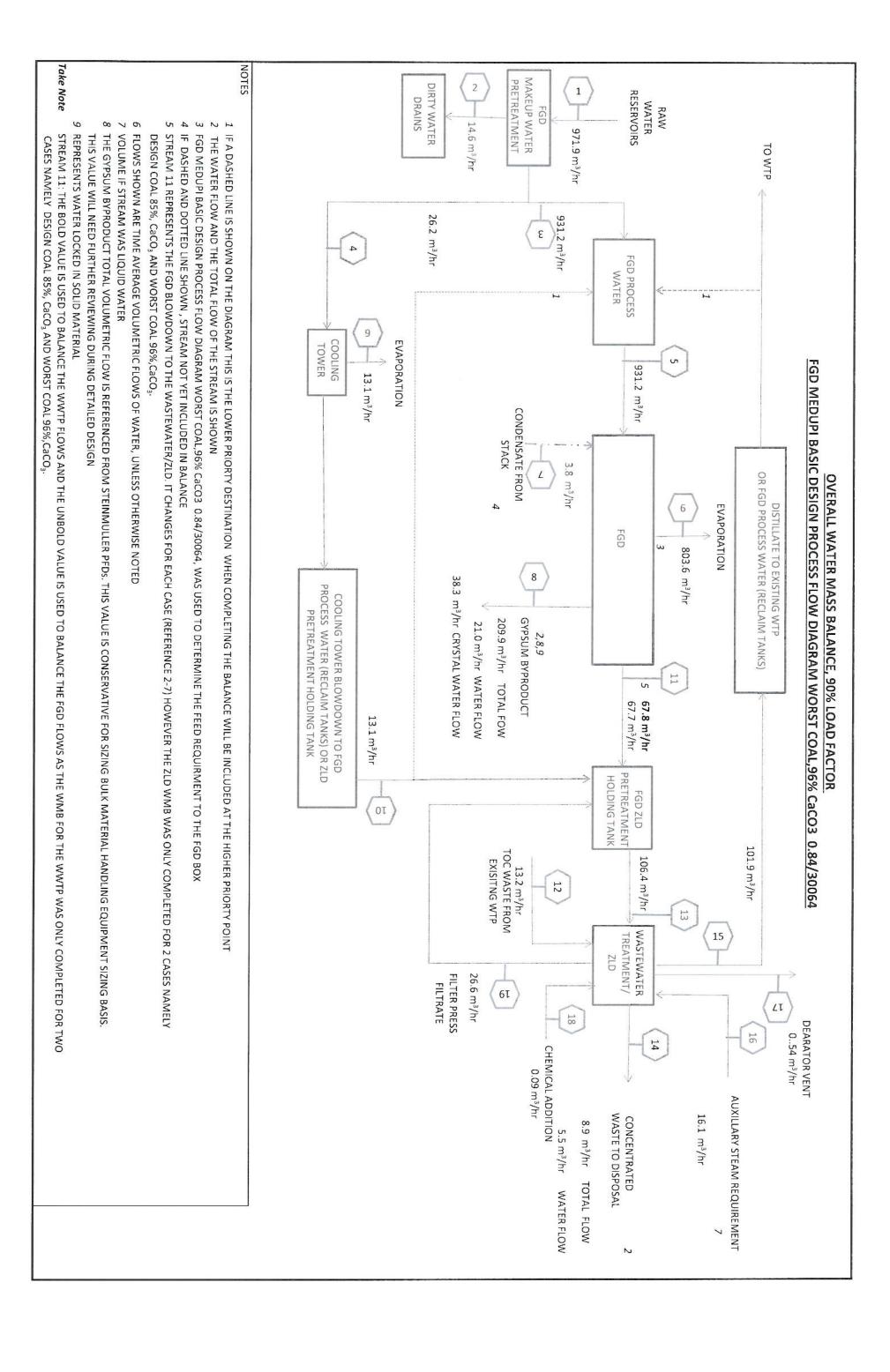


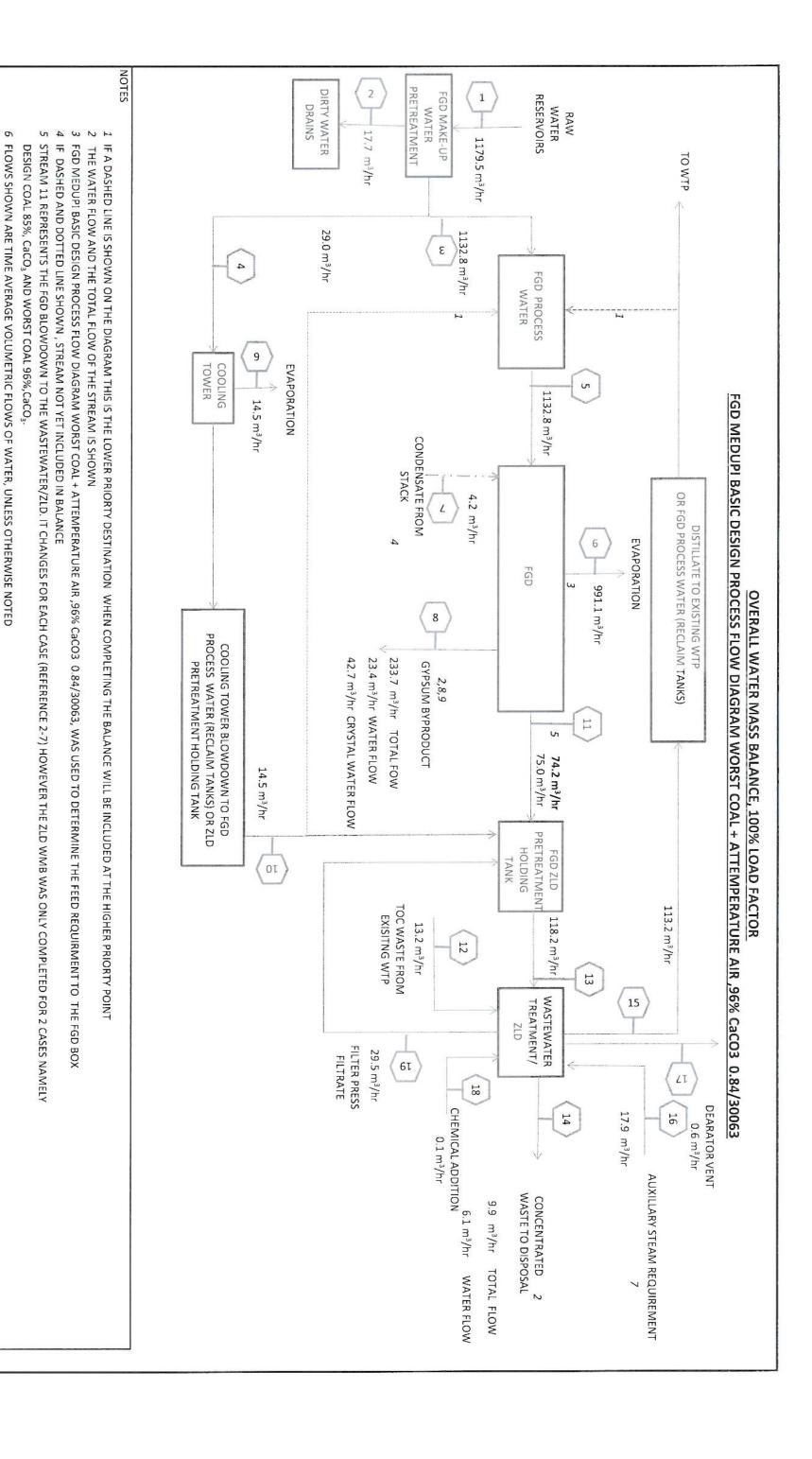












Take Note

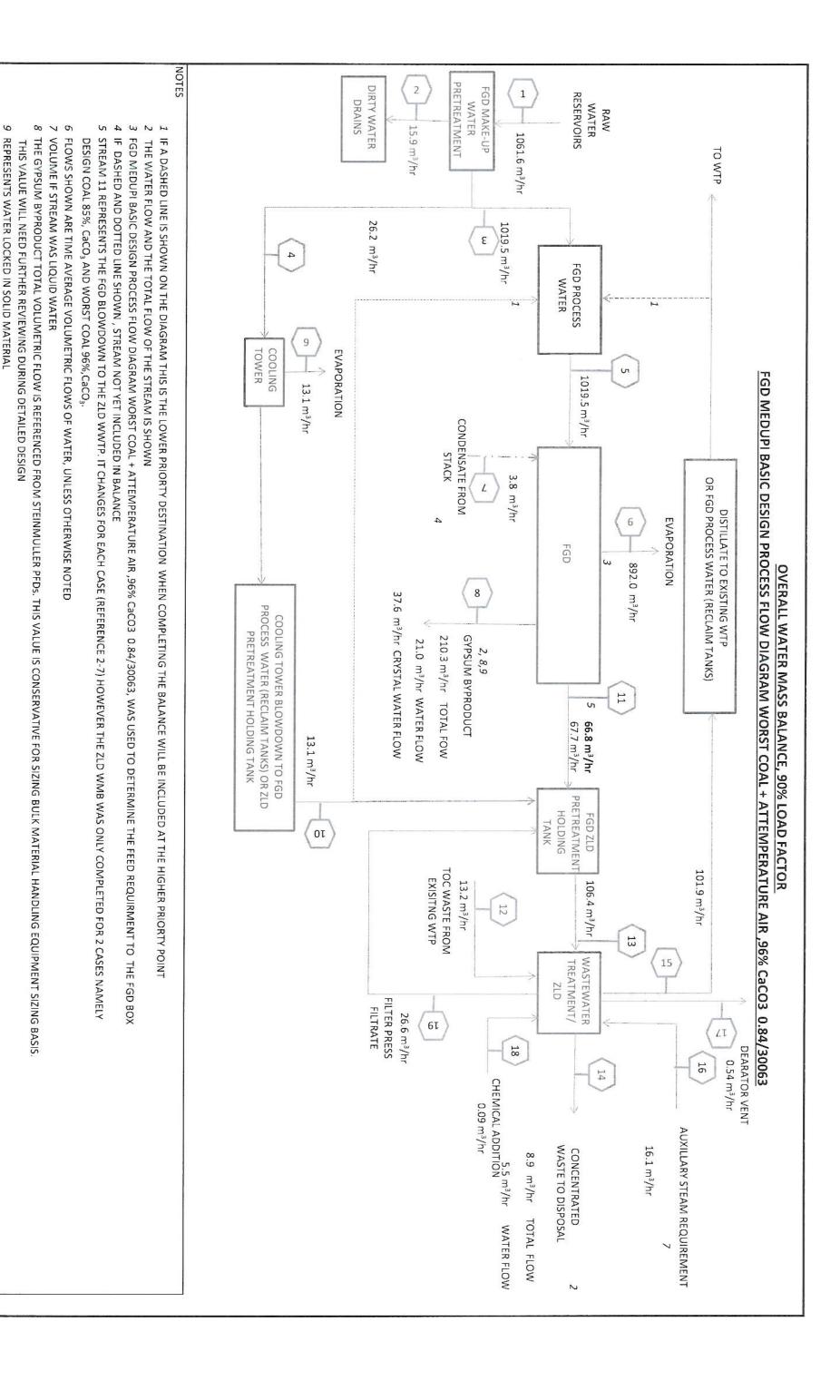
REPRESENTS WATER LOCKED IN SOLID MATERIAL

CASES NAMELY DESIGN COAL 85%, CaCO3 AND WORST COAL 96%,CaCO3.

VOLUME IF STREAM WAS LIQUID WATER

THE GYPSUM BYPRODUCT TOTAL VOLUMETRIC FLOW IS REFERENCED FROM STEINMULLER PFDs. THIS VALUE IS CONSERVATIVE FOR SIZING BULK MATERIAL HANDLING EQUIPMENT SIZING BASIS. THIS VALUE WILL NEED FURTHER REVIEWING DURING DETAILED DESIGN

STREAM 11: THE BOLD VALUE IS USED TO BALANCE THE WWTP FLOWS AND THE UNBOLD VALUE IS USED TO BALANCE THE FGD FLOWS AS THE WMB FOR THE WWTP WAS ONLY COMPLETED FOR TWO



Take Note

CASES NAMELY DESIGN COAL 85%, CaCO3 AND WORST COAL 96%, CaCO3

STREAM 11: THE BOLD VALUE IS USED TO BALANCE THE WWTP FLOWS AND THE UNBOLD VALUE IS USED TO BALANCE THE FGD FLOWS AS THE WMB FOR THE WWTP WAS ONLY COMPLETED FOR TWO